



Shell Global Solutions

Application of detailed kinetic models to ignition processes, limitations

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Scope

- Introduction: industrial need
- Autoignition Temperature (AIT) =
Minimum Ignition Temperature (MIT),
Self-ignition Temperature (SIT),
- Minimum Ignition Energy (MIE)
- Some results (theoretical, experimental) based on EU project (Safekinex) and past work at Delft University of Technology
- Conclusions

Explosion prevention thus

Some of important explosion sensitivity indices are
Auto-ignition Temperature (AIT),

Determination modes: Shock tubes, Rapid compression machines, Constant volume bombs

Practical challenges τ , mixing, h

Minimum Ignition Energy (MIE)

Ample evidence these indices are affected e.g. by:

- | | | |
|--------------------------|------------------|------------------|
| • Pressure \uparrow | AIT \downarrow | MIE \downarrow |
| • Temperature \uparrow | AIT NA | MIE \downarrow |
| • Heat loss \uparrow | AIT \uparrow | MIE \uparrow |
- (turbulence, apparatus conditions)

Can one relay on ambient conditions data?

Current status

Determination practice

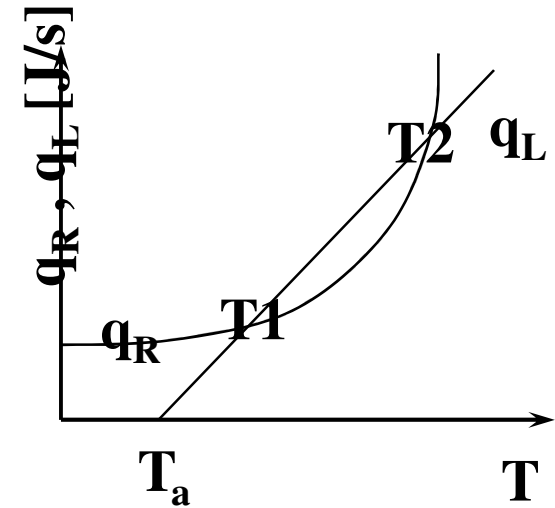
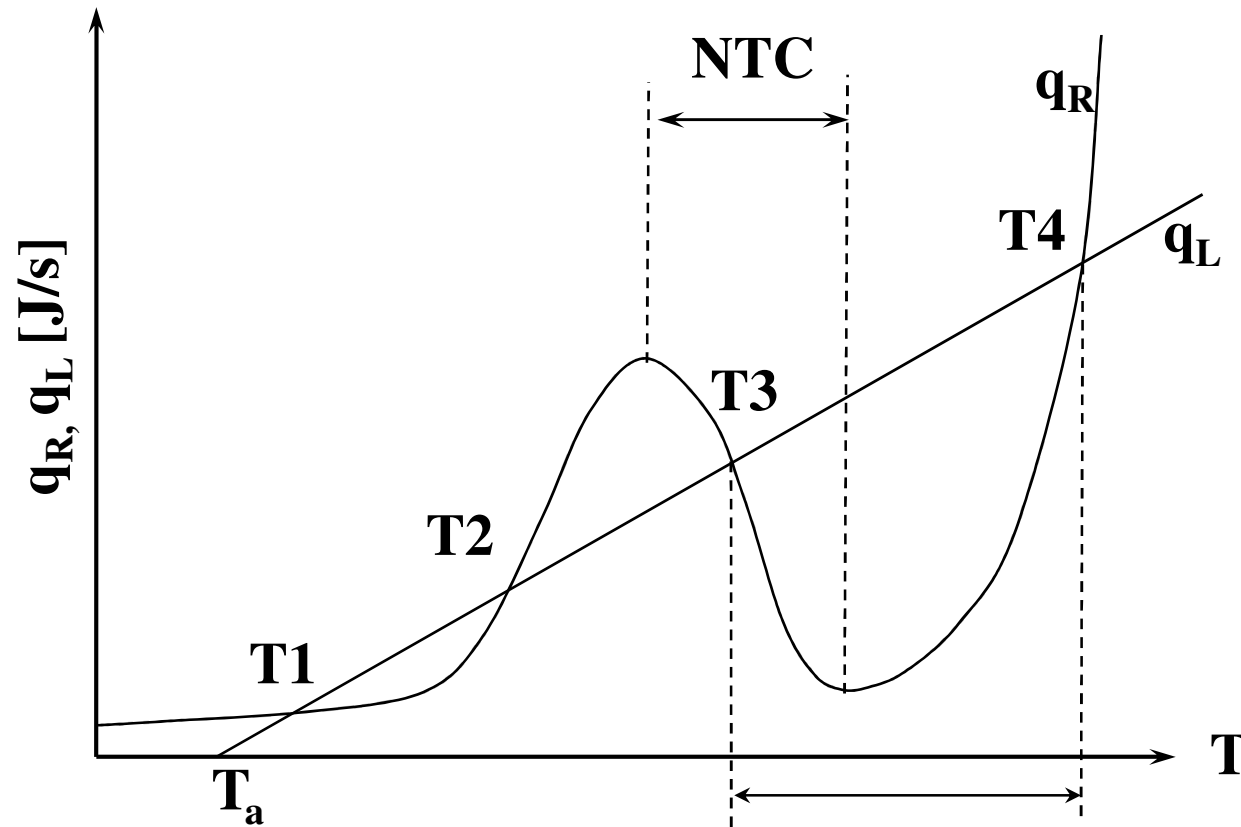
Standards exist for

AIT, constant volume bomb only, ambient pressure

MIE, ambient pressure and temperature

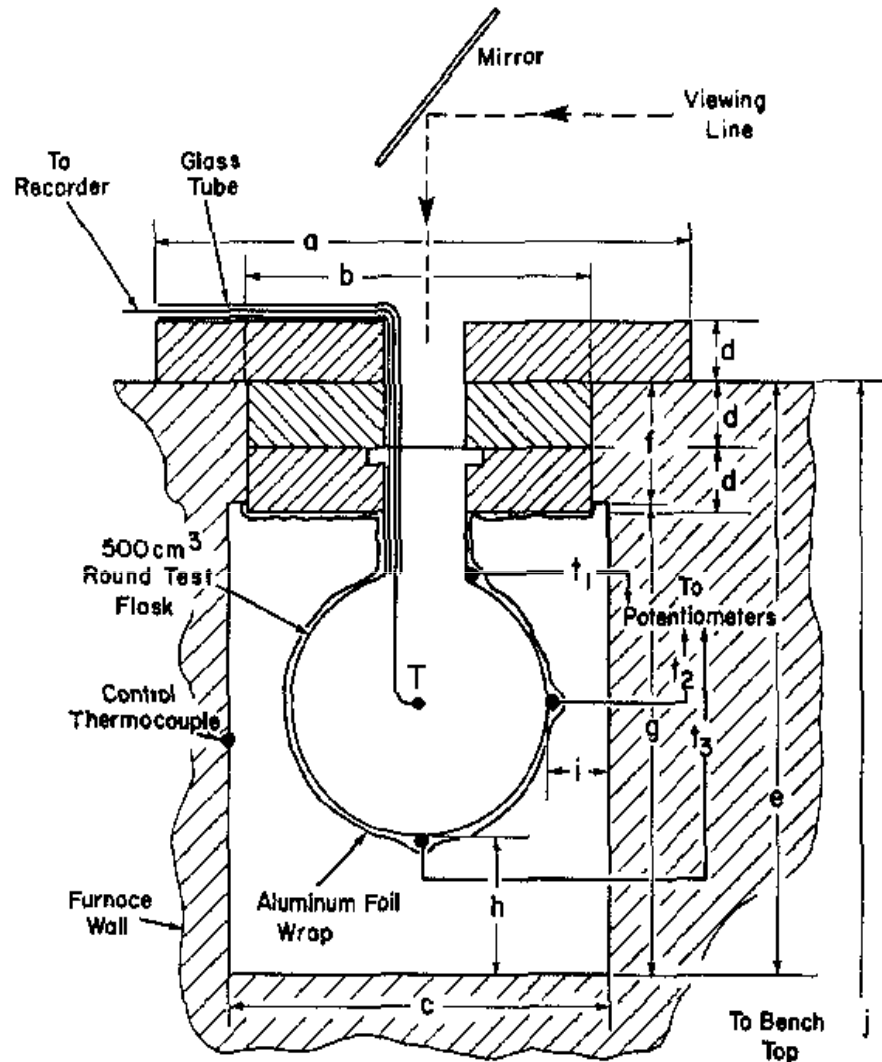
Is that sufficient? !

Inherent problem with AIT: heat loss



Extra safety margin ?

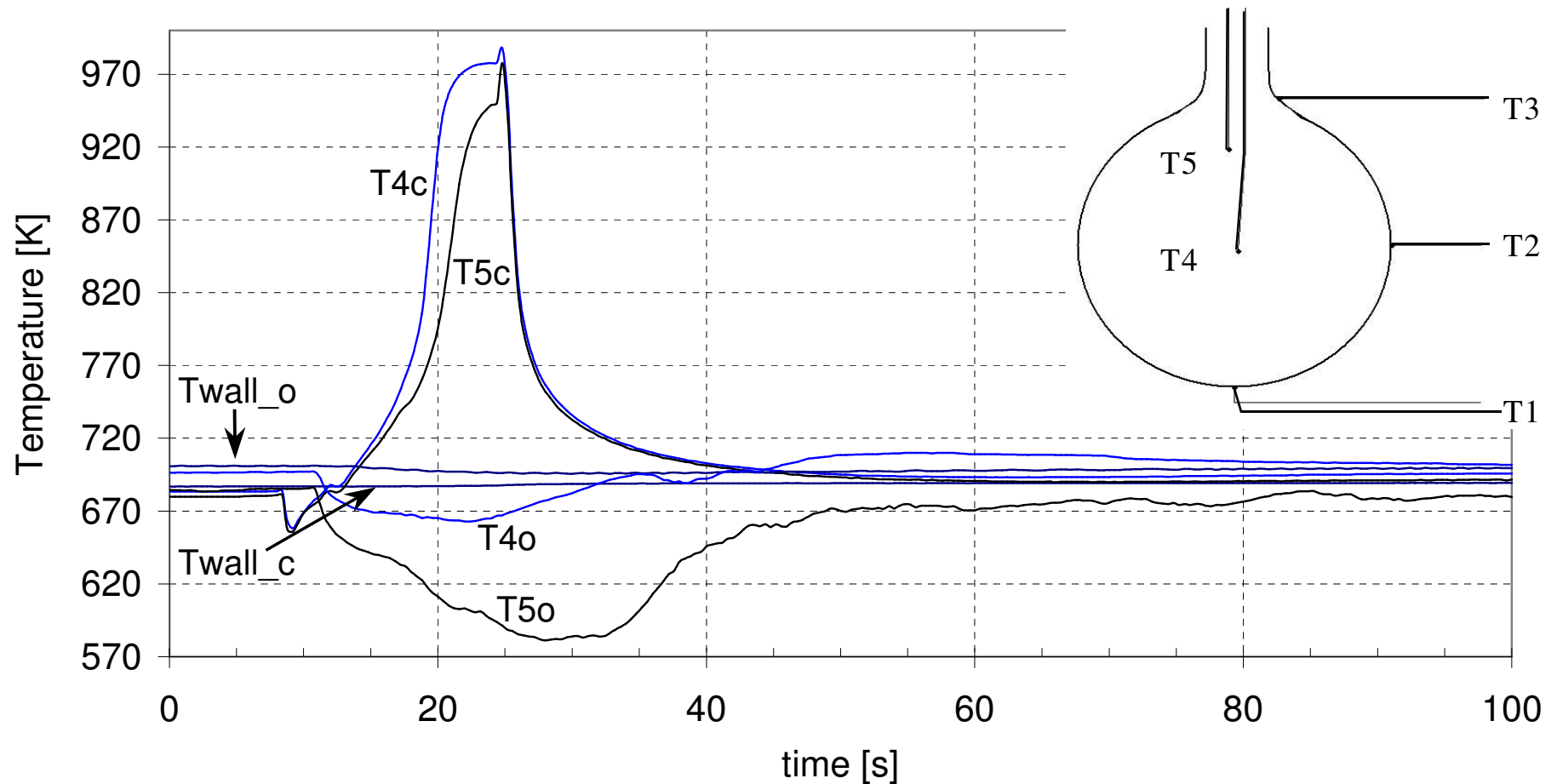
AIT Constant Volume Bomb ASTM E 659 – 78 (2005)



- Atmospheric pressure
- T max approximately 600 °C
- 500 ml borosilicate glass
- 10 minutes observation
- Liquid samples
- Open vessel
- Ignition appearance of a flame accompanied by a sharp T rise

**heat loss
natural convection induced**

Open-closed flask CH₄-C₂H₄-O₂ mixtures



Clearly different combustion phenomena are observed depending on the closure mode of the vessel

Modes of heat transfer - Rayleigh Number (Ra)

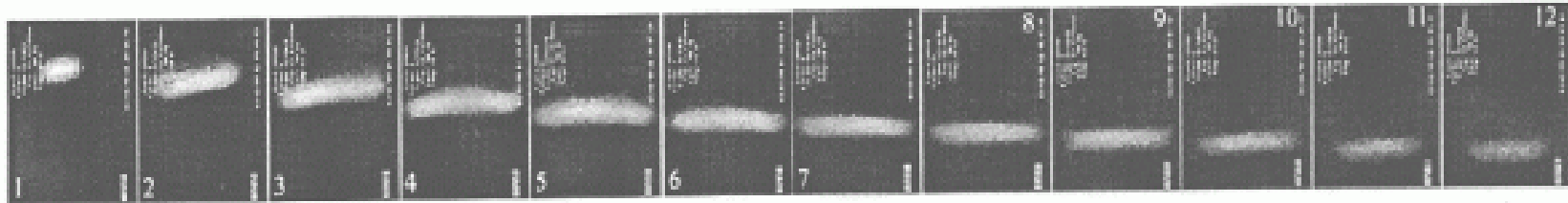
$$Ra = g \beta r^3 C_p \rho^2 \Delta T / \lambda \eta$$

Ra < 600: conduction

600 < Ra < 10⁴ : conduction and convection

Ra > 10⁴ : convection

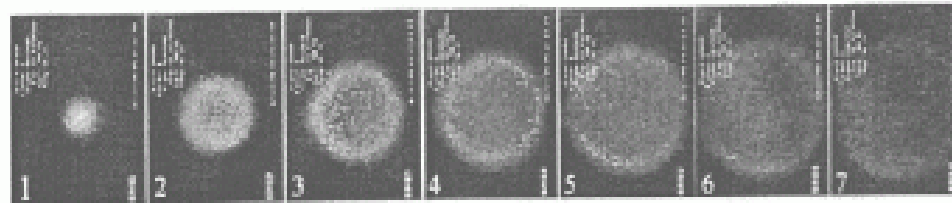
1g



(a)

~0g

(b)

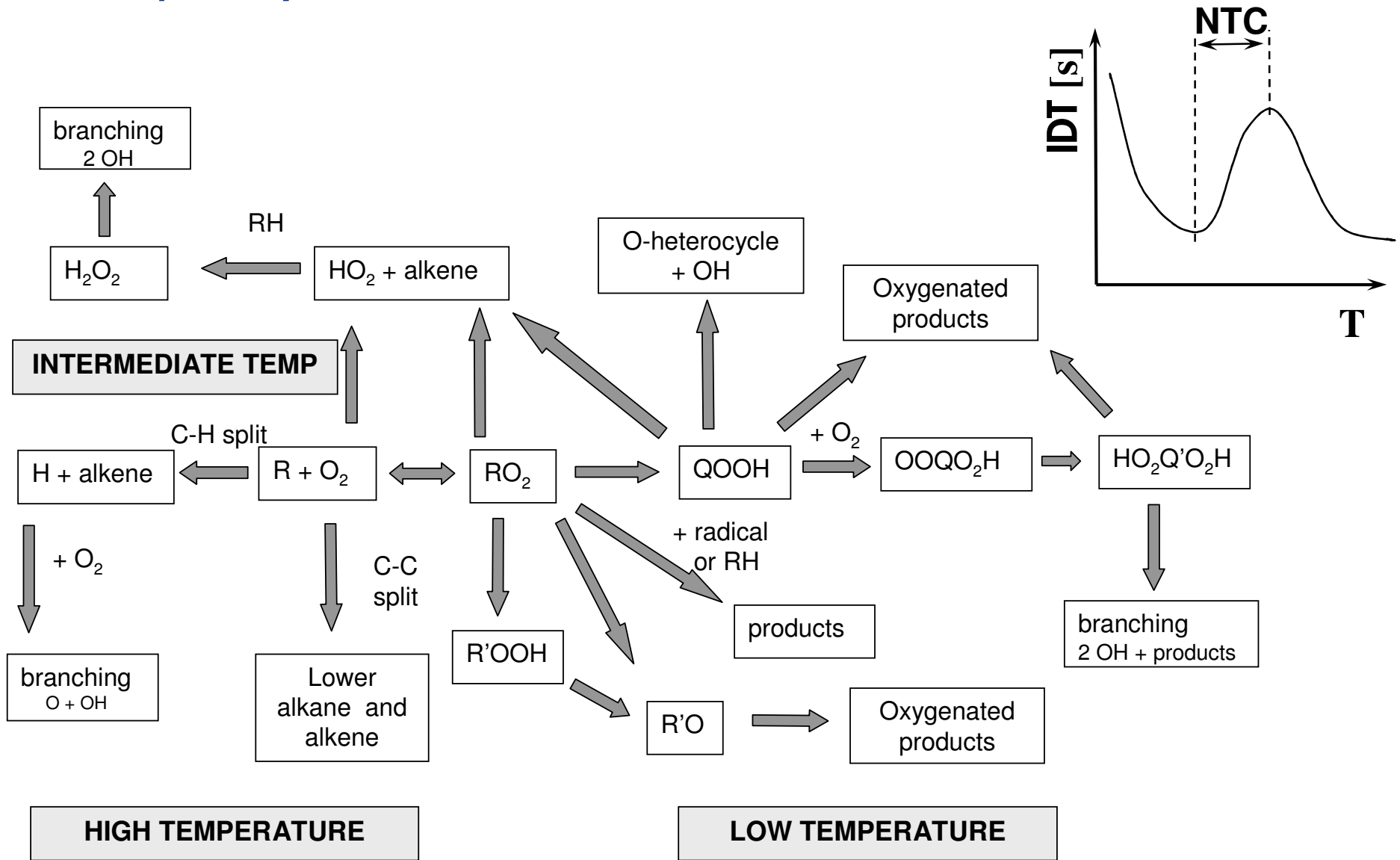


Natural convection assists laboratory SIT experiment: (1g) => importance assessment of timescales (chemical reaction, heat conduction, natural convection, heat diffusion ΔT) => complexity

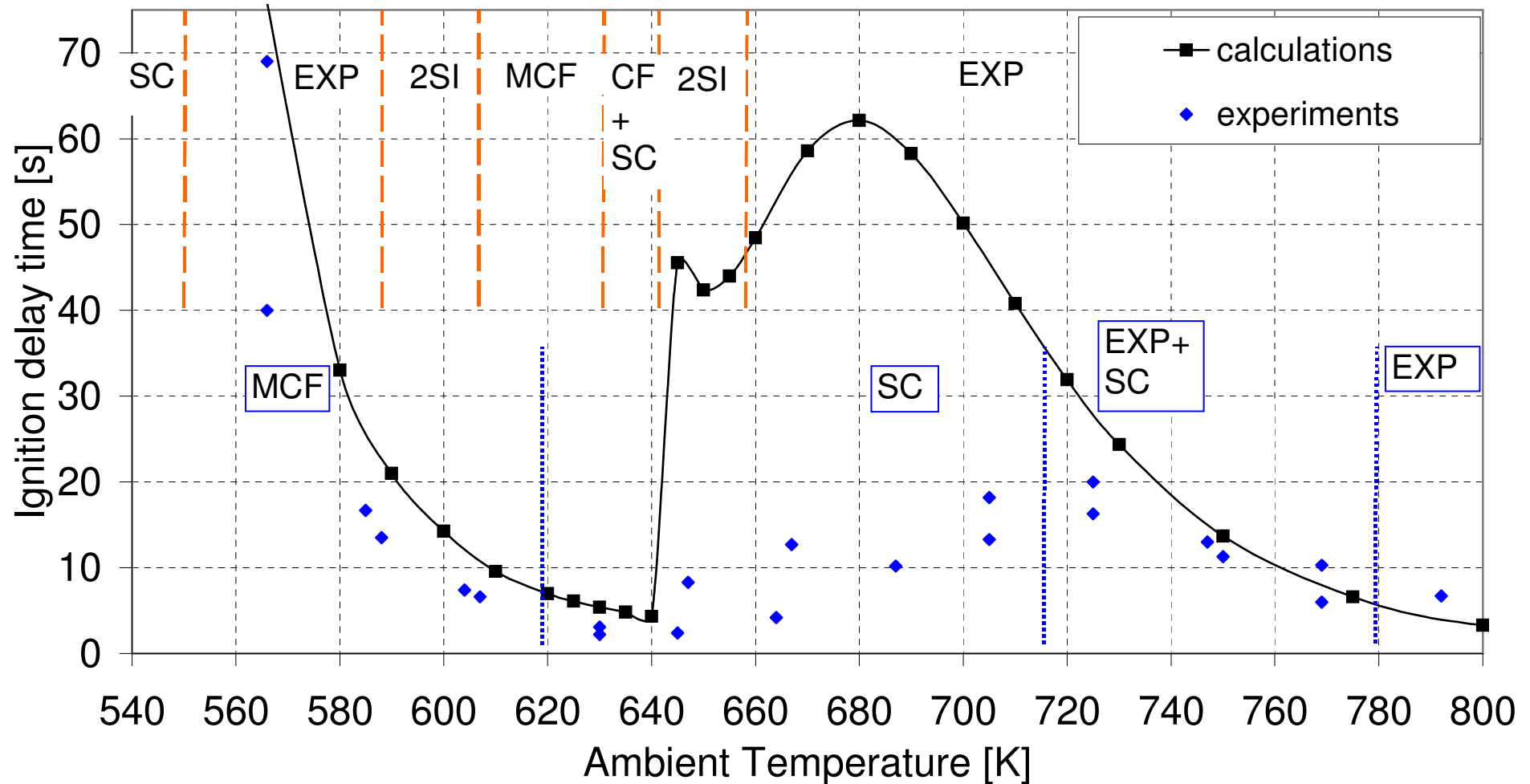
Work in progress

University of Cambridge under Dr S. Cardoso

Complexity of kinetic: Combustion kinetics with respect to T

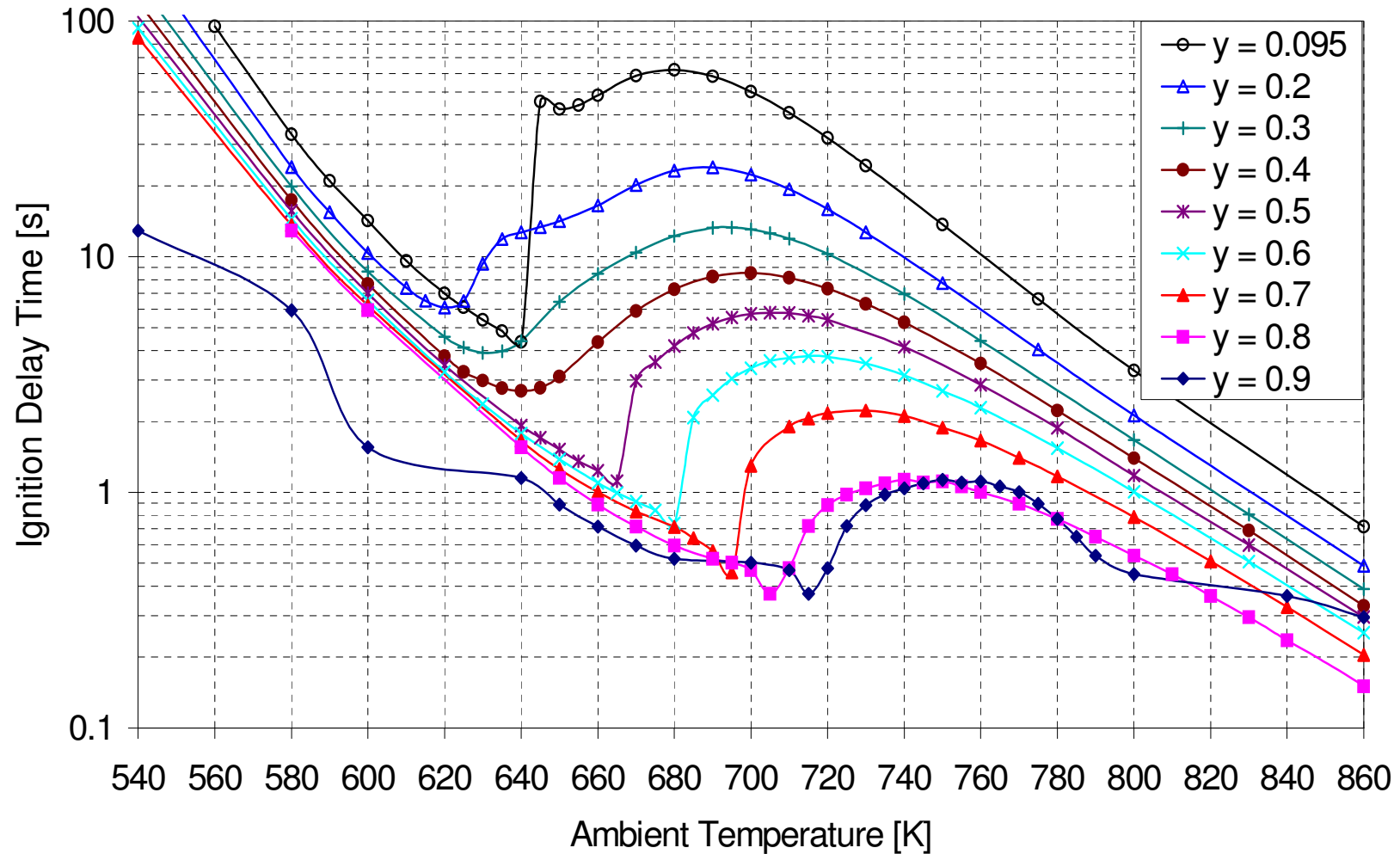


Comparison between experiments and numerical calculations; combustion phenomena



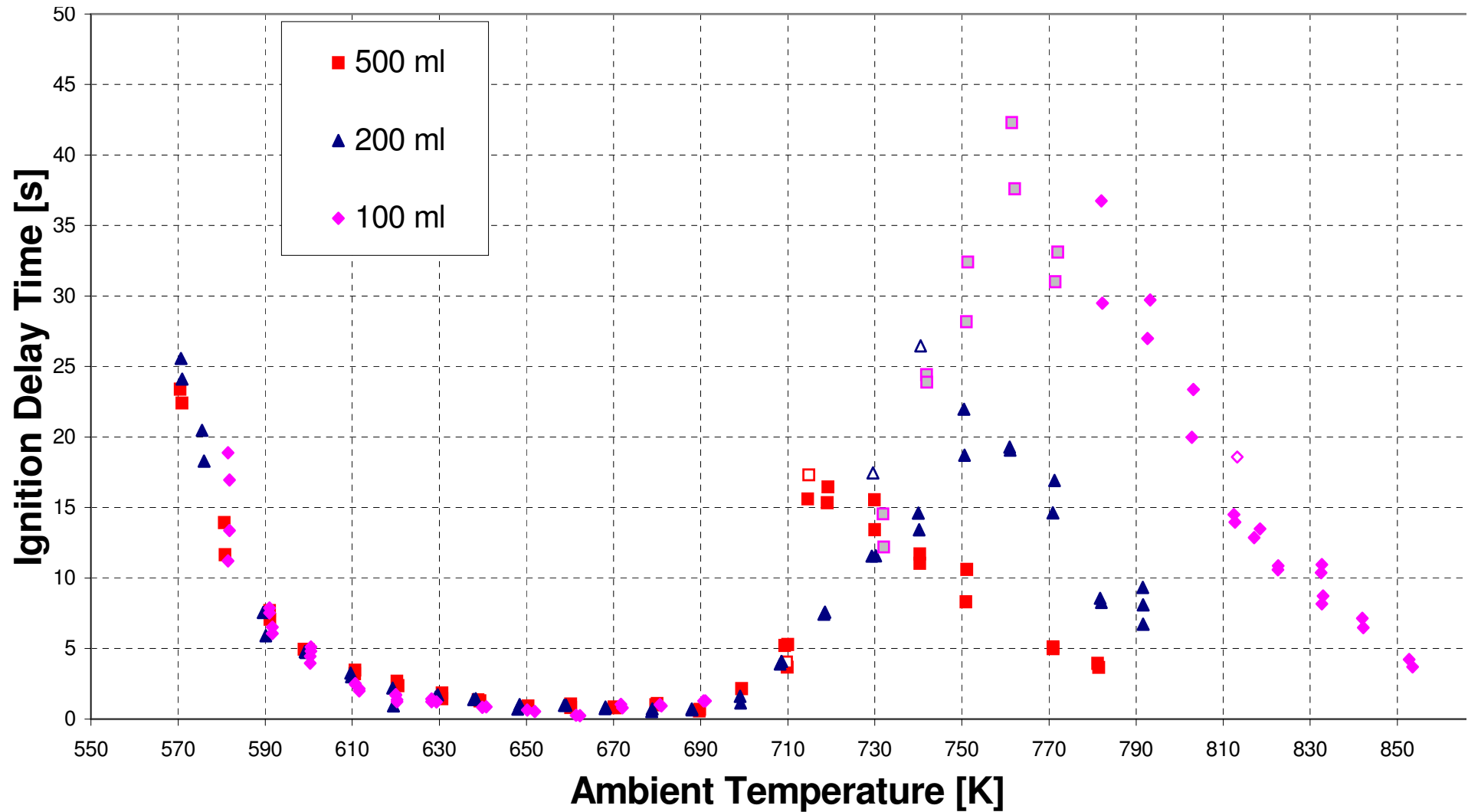
Difference in NTC => importance of interaction between physics and kinetic

Effect of mixture composition on NTC

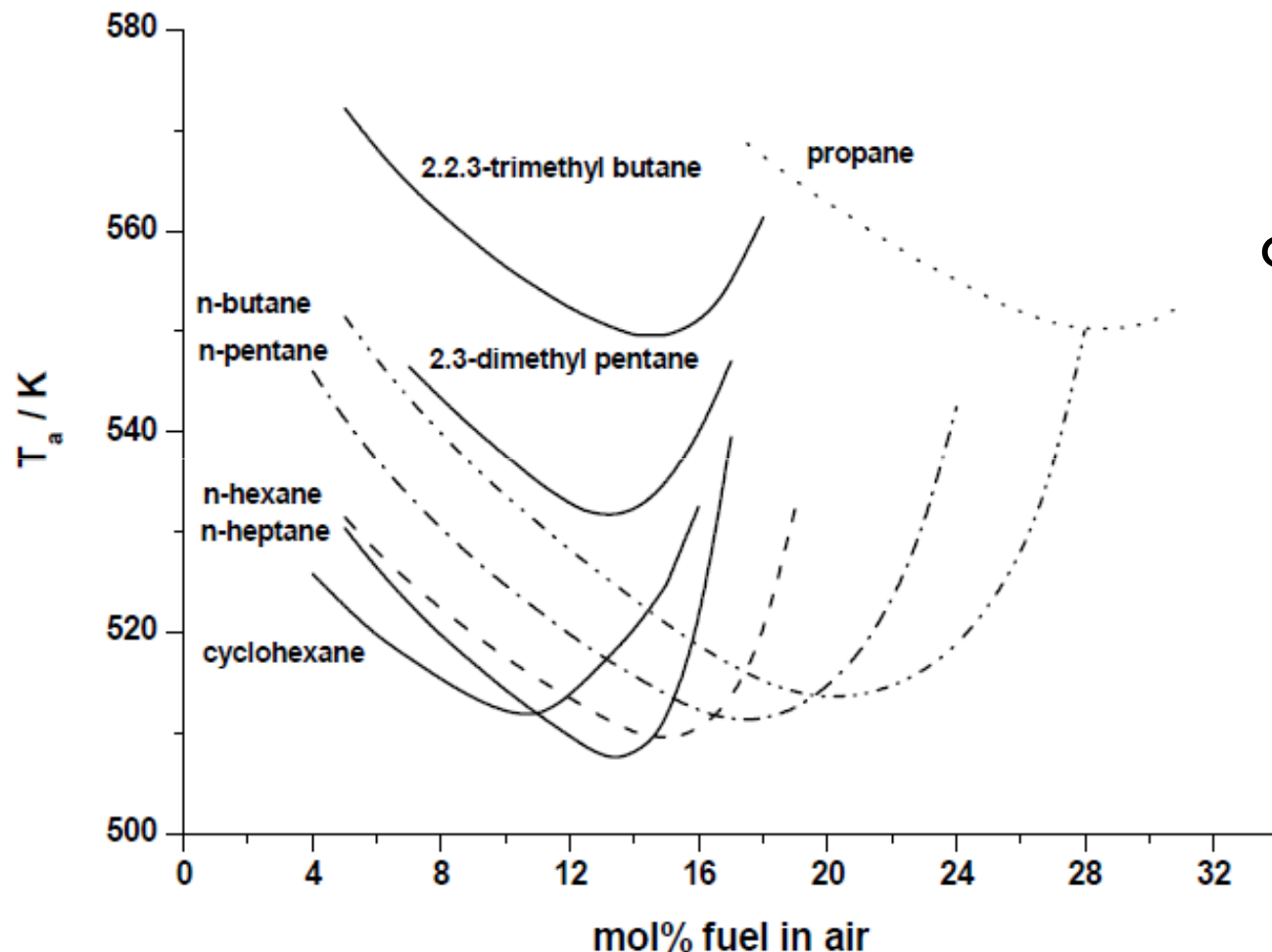


Logarithmic scale presentation of the negative temperature coefficient of various n-butane-air mixtures, $P_0 = 1$ bara, mole fraction of n-butane is in the legend, calculations.

Auto-ignition times for different volumes; 100, 200, 500 ml



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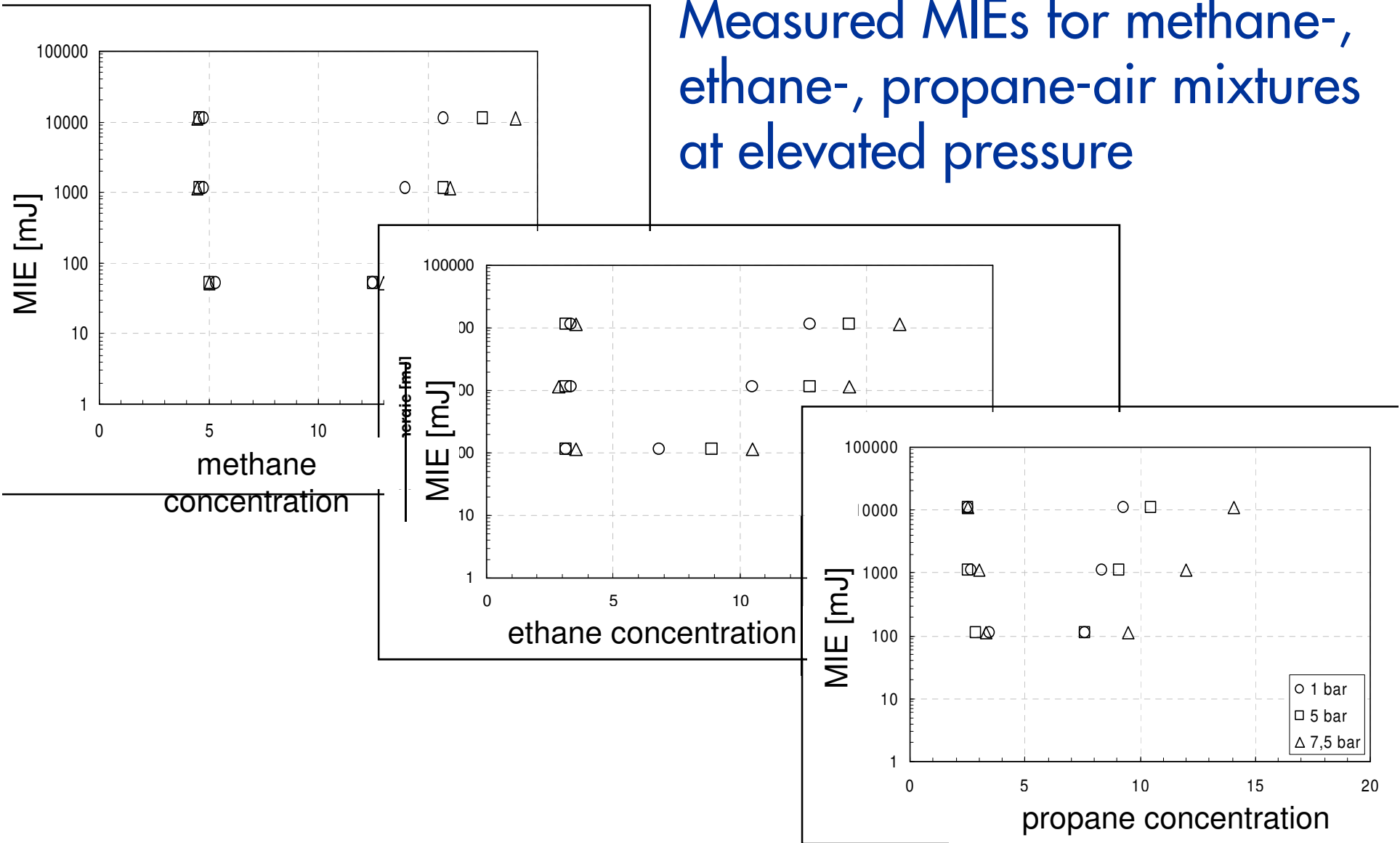


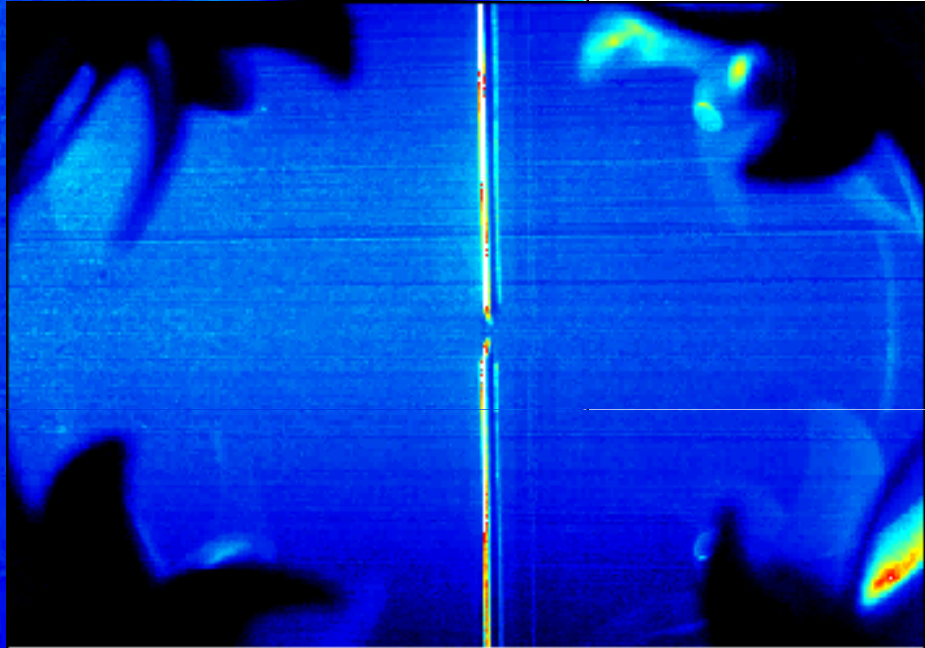
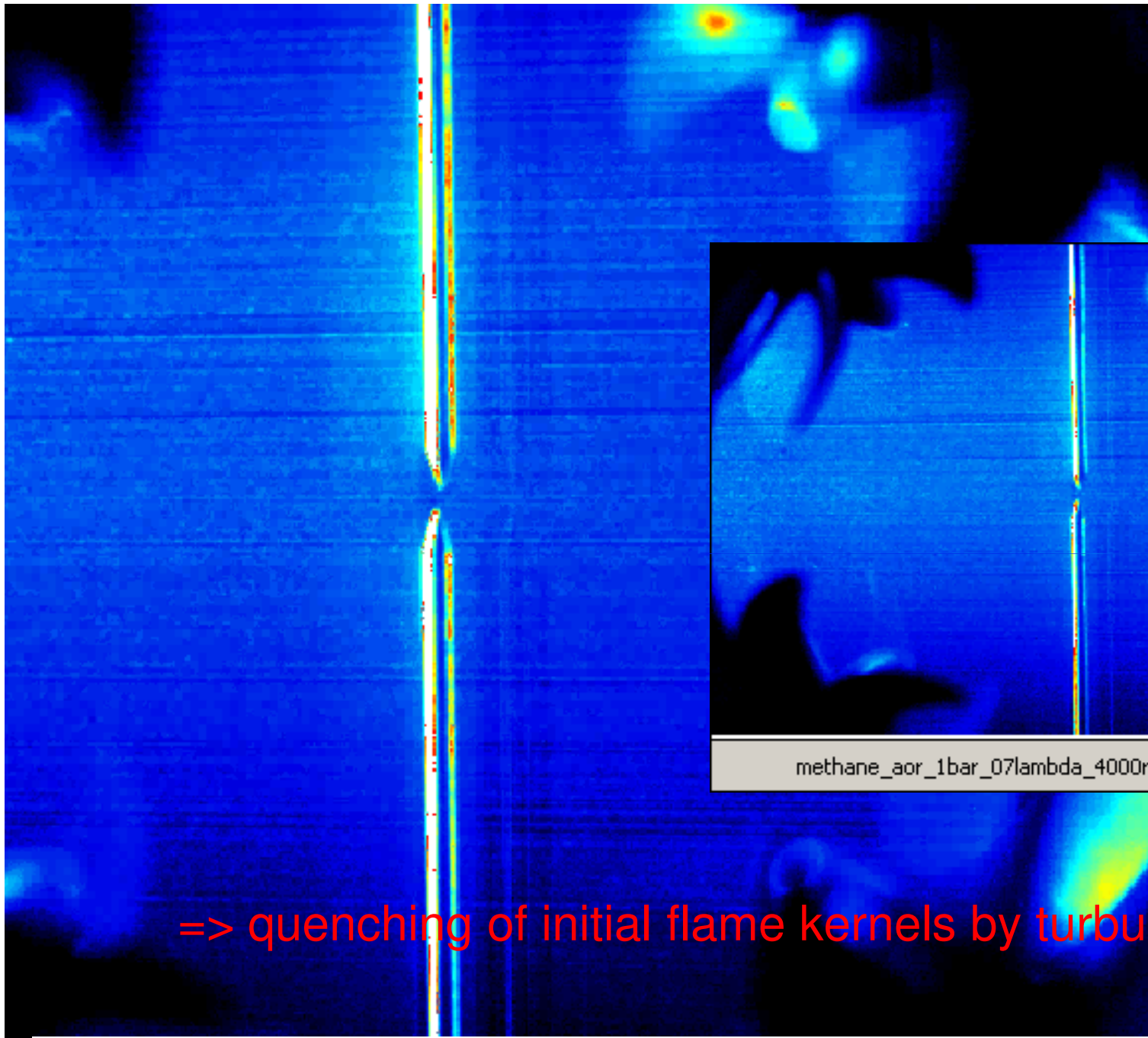
Theoretically
calculated AIT and
SIT using EXGAS
input;

Source: Safekinx
Del. 38
Leeds University
Prof M. Fairweather
Prof J. Griffiths at al.

Minimum Ignition Energy

Measured MIEs for methane-, ethane-, propane-air mixtures at elevated pressure





methane_aor_1bar_07lambda_4000rpm_notignited.avi

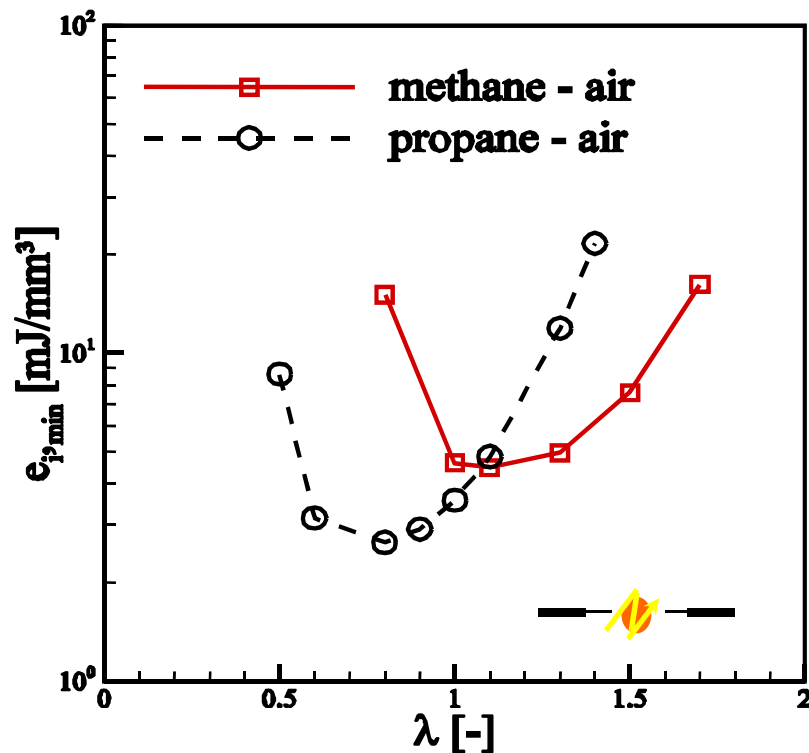
=> quenching of initial flame kernels by turbulence

Simulation Tool: INSFLA and COSILAB:

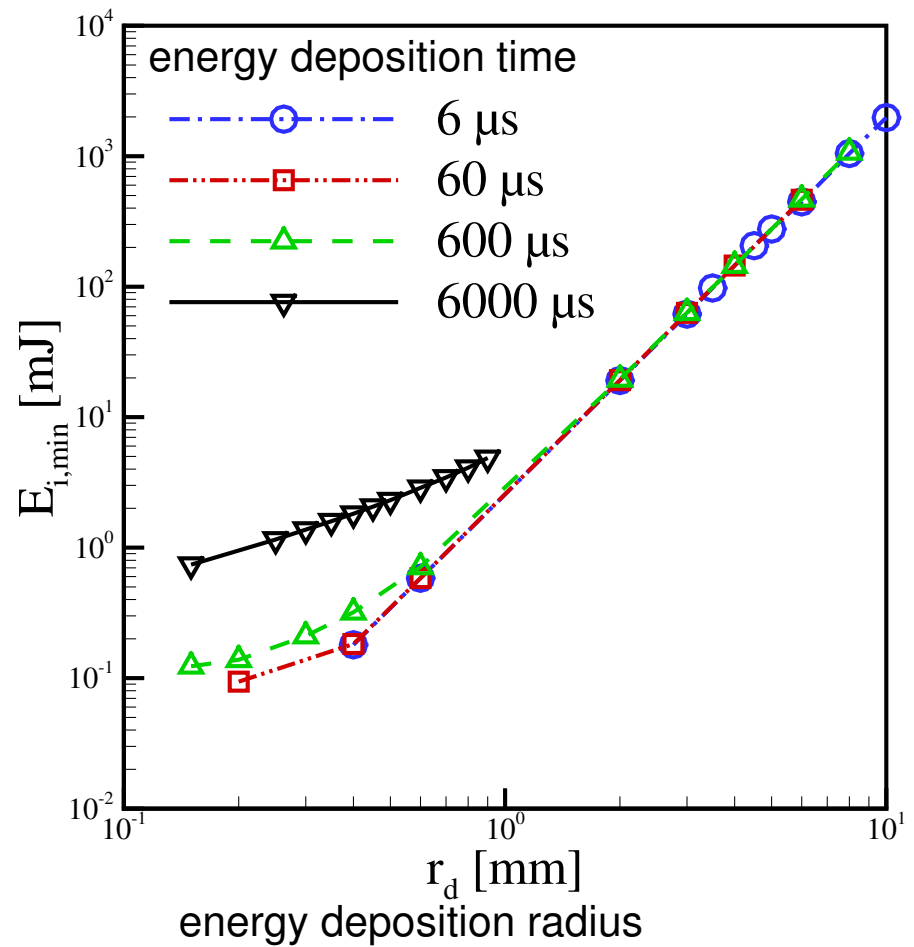
- one-dimensional
- solving unstead flames
- detailed kinetic scheme (HTOM)

Influence of energy deposition time and radius on the MIE

Minimum ignition energy



Simulated MIEs for methane- and propane-air mixtures at atmospheric conditions



Conclusions

1. Self-ignition phenomena in complex (realistic) conditions.
2. Measurement of AIT, MIE at elevated (process) conditions is a challenge
3. Better understanding
4. Good resolution on kinetic scheme or flow.

Thank you for your attention

Questions ?